



# STUDY OF THE PROCESS OF DECOMPOSITION OF TRICALCIUM PHOSPHATE BY PHOSPHORIC ACID WITH PARTIAL REPLACEMENT OF P2O5 BY SULFURIC ACID IN THE PRESENCE OF AMMONIUM NITRATE

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## Annotation

In the article, the study of the decomposition process of tricalcium phosphate with a mixture of thermal phosphoric acid with partial replacement of phosphoric acid with sulfuric acid in the presence of ammonium nitrate and their joint presence, the study of the conversion of calcium sulfate to ammonium sulfate.

**Keywords:** Uzbekistan, tricalcium phosphate, decomposition of tricalcium phosphate, thermal phosphoric acid, sulfuric acid, agrochemical complex, macronutrient, nitrogen, phosphorus, potassium, calcium, magnesium, sulfur, decomposition coefficient, SO<sub>3</sub> extraction rate into aqueous solution, water-soluble form, ammonium nitrate, rheological properties.

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## INTRODUCTION.

The agrochemical complex is a key component of the economic development of the Republic, on the development of which the well-being of the population depends. In this regard, providing the agro-industrial complex with the necessary plant protection products, plant growth and development stimulants, mineral and organo-mineral fertilizers in a wide range, with different ratios of the main macronutrients - nitrogen, phosphorus, potassium, calcium, magnesium, sulfur is an important direction in increasing productivity. crops.

Increasing the rate of application of mineral fertilizers no longer contributes to an increase in yield. In addition to nitrogen, phosphorus and potassium, plants need

calcium, magnesium, sulfur and trace elements. The presence in the Republic of a powerful industrial base for the production of mineral fertilizers, including single phosphate fertilizers, effective for application under autumn plowing, is directly related to the introduction of scientific achievements in the processing of phosphate raw materials into production, with the expansion of their range and the content of macro and microelements.

In Uzbekistan, as concentrated phosphorus fertilizers, at present, mainly ammophos is used, obtained from phosphorites of the Central Kyzylkum. As a result of the use of ammophos, the amount of soluble and assimilated by plants calcium, magnesium and sulfur compounds introduced into the soil



annually decreases, which in turn leads to a deficiency of these elements in the body of animals and plants.

In this aspect, an important task is to substantiate scientific and technical solutions for the development of technologies for single and concentrated phosphate fertilizers with a water-soluble form of sulfates.

**MATERIALS AND METHODS.** For the theoretical justification of the processing of phosphorites into single phosphate fertilizers with phosphoric acid, with partial replacement of P<sub>2</sub>O<sub>5</sub> phosphoric acid with sulfuric acid, studies were carried out on the decomposition of tricalcium phosphate by thermal phosphoric acid containing 20% P<sub>2</sub>O<sub>5</sub> with the replacement of 10, 20 and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid at a total stoichiometric the norm of acids, at a temperature of 80°C and a process duration of 2 hours.

The study of the decomposition process of tricalcium phosphate was also carried out with a more concentrated thermal phosphoric acid, and the replacement of 10, 20 and 30% P<sub>2</sub>O<sub>5</sub> with H<sub>2</sub>SO<sub>4</sub> with a concentration of 91.8% in a laboratory installation under periodic conditions. To do this, a certain amount of phosphoric acid was introduced into a thermostatically controlled reactor equipped with a paddle stirrer, and after reaching a

predetermined temperature, the calculated amount of tricalcium phosphate was dosed. After a certain period of time, pulp samples were taken for analysis to determine the content of various forms of P<sub>2</sub>O<sub>5</sub>, CaO, SO<sub>3</sub> and to calculate the coefficient of decomposition of tricalcium phosphate, the coefficients of extraction of CaO and SO<sub>3</sub> into the liquid phase.

**DISCUSSION.** To reveal the role of sulfuric acid in the partial replacement of P<sub>2</sub>O<sub>5</sub> thermal phosphoric acid by sulfuric acid, the decomposition of tricalcium phosphate by a mixture of acids was studied when 10, 20, and 30% P<sub>2</sub>O<sub>5</sub> were replaced by sulfuric acid.

Chemical analysis of the pulp for the content of the main components showed that when tricalcium phosphate is decomposed by thermal phosphoric acid with an initial concentration of 18.25% P<sub>2</sub>O<sub>5</sub> and containing 1.14% SO<sub>3</sub>, the content of P<sub>2</sub>O<sub>5total</sub> is 23.25%, P<sub>2</sub>O<sub>5assimilable</sub> 21.69%, P<sub>2</sub>O<sub>5water-soluble</sub> 19.83% . With an increase in the amount of replacement of P<sub>2</sub>O<sub>5</sub> with sulfuric acid, the content of P<sub>2</sub>O<sub>5total</sub> in the product decreases to 21.83% and 20.39%, respectively, when replacing 20 and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid. The decomposition ratio of tricalcium phosphate increases from 81.21% to 87.50% and 94.58%. The results obtained are presented in table 1.

**Table 1.**

**Influence of partial replacement of phosphoric acid by sulfuric acid on the chemical composition of the pulp.**

№	Performance	The content of components in the pulp, wt. %								
		when replacing H <sub>3</sub> PO <sub>4</sub> with H <sub>2</sub> SO <sub>4</sub> , %								
		10	20	30	10	20	30	10	20	30
1.	Initial concentration of P <sub>2</sub> O <sub>5</sub> in WPPA, %	18,25	16,45	14,60	27,38	24,68	21,90	36,50	32,90	29,20
2.	Initial concentration of SO <sub>3</sub> in WPPA, %	1,14	2,32	3,53	1,71	3,48	5,30	2,28	4,64	7,06
3.	Content in the pulp:									
	P <sub>2</sub> O <sub>5</sub> (total), %	23,25	21,83	20,39	31,97	30,00	27,99	39,36	36,90	34,40
	P <sub>2</sub> O <sub>5</sub> (assimilable), %	21,69	20,78	19,85	30,15	28,62	27,04	38,53	36,38	34,02
	P <sub>2</sub> O <sub>5</sub> (water-soluble), %	19,83	19,25	18,43	26,95	26,82	25,64	34,99	33,80	32,10



	SO <sub>3</sub> (total), %	0,93	1,89	2,86	1,28	2,60	3,95	1,58	3,20	4,85
	SO <sub>3</sub> (water-soluble), %	0,37	0,59	0,69	0,52	0,82	0,94	0,65	0,97	1,16
	CaO (total), %	9,82	9,94	10,09	13,51	13,65	13,80	16,63	16,79	16,96
	CaO (total), %	2,78	2,66	2,27	4,01	3,70	2,83	5,01	4,28	3,59
	влага, %	56,96	57,60	58,29	40,78	41,75	42,72	27,18	28,35	29,63
4.	(P <sub>2</sub> O <sub>5</sub> <sub>assimilable</sub> :P <sub>2</sub> O <sub>5</sub> <sub>total</sub> )×100, %	93,29	95,19	97,35	94,30	95,40	96,60	97,90	98,60	98,90
5.	(P <sub>2</sub> O <sub>5</sub> <sub>water-soluble</sub> :P <sub>2</sub> O <sub>5</sub> <sub>total</sub> )×100, %	85,29	88,18	90,39	84,30	89,40	91,60	88,90	91,60	93,31
6.	K <sub>5</sub> of P <sub>2</sub> O <sub>5</sub> <sub>assimilable</sub> , %	81,21	87,50	94,58	84,04	88,05	93,05	94,12	96,36	97,75
7.	K <sub>ext</sub> for CaO in aqueous solution, %	28,31	26,76	22,50	29,68	27,10	20,51	30,13	25,49	21,17
8.	Degree of extraction of SO <sub>3</sub> into aqueous solution (Degree of conversion of calcium sulfate), %	39,79	31,22	24,13	40,62	31,54	23,80	41,14	30,31	23,92

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When using more concentrated phosphoric acid, the content of the total form of SO<sub>3</sub> is 1.28-4.85% and water 0.52-1.16%. The recovery factor of SO<sub>3</sub> into the liquid phase, with an increase in the proportion of H<sub>2</sub>SO<sub>4</sub>, decreases and amounts to 39.79-24.13% when replacing 10% P<sub>2</sub>O<sub>5</sub> with H<sub>2</sub>SO<sub>4</sub>, 40.63-23.80% when replacing 20% and 41.14-23, 92% with 30% replacement. This indicates that with an increase in the content of H<sub>2</sub>SO<sub>4</sub> in phosphoric acid, the proportion of the water-soluble form of SO<sub>3</sub> in the pulp decreases.

Table 2 shows the results of the process of drying the decomposition products of tricalcium phosphate with 20% thermal phosphoric acid when replacing 10%, 20% and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid.

The use of more concentrated phosphoric acid with the replacement of 10, 20 and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid makes it possible to obtain a product with a higher degree of decomposition.

**Table 2.**  
**Influence of partial replacement of phosphoric acid by sulfuric acid on the chemical composition of the product**

№	Performance	Content of components, wt. %								
		when replacing H <sub>3</sub> PO <sub>4</sub> with H <sub>2</sub> SO <sub>4</sub> , %								
		10	20	30	10	20	30	10	20	30
1.	Initial concentration of P <sub>2</sub> O <sub>5</sub> in WPPA, %	18,25	16,45	14,60	27,38	24,68	21,90	36,50	32,90	29,20
2.	Initial concentration of SO <sub>3</sub> in WPPA, %	1,14	2,32	3,53	1,71	3,48	5,30	2,28	4,64	7,06
3.	Content in the product:									
	P <sub>2</sub> O <sub>5</sub> (total), %	53,44	50,36	48,51	53,00	50,14	50,07	53,14	49,86	48,02
	P <sub>2</sub> O <sub>5</sub> (assimilable), %	50,22	48,37	47,66	50,53	48,08	48,61	52,26	49,46	47,92



	P <sub>2</sub> O <sub>5</sub> (water-soluble), %	46,12	44,89	44,26	45,17	45,15	46,19	47,42	46,19	45,09
	SO <sub>3</sub> (total), %	2,14	4,36	6,80	2,20	4,35	6,73	2,13	4,32	6,77
	SO <sub>3</sub> (water-soluble), %	0,86	1,42	1,82	0,94	1,42	1,67	0,90	1,36	1,75
	CaO (total), %	22,57	22,93	24,00	22,40	22,81	24,69	22,45	22,69	23,67
	CaO (total), %	6,62	6,24	5,58	6,78	6,48	5,38	6,99	6,02	5,28
	влага, %	1,08	2,18	0,77	1,83	2,64	2,41	1,69	3,18	1,77
4.	(P <sub>2</sub> O <sub>5</sub> <sub>assimilable</sub> :P <sub>2</sub> O <sub>5</sub> <sub>total</sub> )×100, %	93,97	96,05	98,25	95,34	95,89	97,08	98,35	99,20	99,80
5.	(P <sub>2</sub> O <sub>5</sub> <sub>water-soluble</sub> :P <sub>2</sub> O <sub>5</sub> <sub>total</sub> )×100, %	86,30	89,13	91,24	85,23	90,05	92,25	89,25	92,64	93,90
6.	K <sub>s</sub> of P <sub>2</sub> O <sub>5</sub> assimilable, %	83,12	89,74	96,42	86,95	89,32	94,03	95,38	97,92	99,51
7.	K <sub>ext</sub> for CaO in aqueous solution, %	29,33	27,21	23,25	30,27	28,41	21,79	31,13	26,53	22,31
8.	Degree of extraction of SO <sub>3</sub> into aqueous solution (Degree of conversion of calcium sulfate), %	40,19	32,57	26,76	42,73	32,64	24,81	42,25	31,48	25,85

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The highest results of the decomposition coefficient were obtained when phosphoric acid was evaporated to a content of 32.90% P<sub>2</sub>O<sub>5</sub> and 4.64% SO<sub>3</sub>, as well as up to 29.20% P<sub>2</sub>O<sub>5</sub> and 7.06% SO<sub>3</sub>, respectively, 97.92% and 99.51% .

In the works of K. Gafurov, I.T. Shamshidinov, the possibility of evaporating WPPA from phosphorites of Karatau and Central Kyzylkum to a content of 40-45% P<sub>2</sub>O<sub>5</sub> and obtaining an acid with acceptable physico-chemical characteristics by introducing ammonium nitrate into the initial acid was shown.

The introduction of ammonium nitrate into the composition of WPPA not only

improves the rheological properties of stripped off acids, but also promotes the activation of phosphoric acid, which is reflected in the intensification of the process of decomposition of phosphate raw materials. Taking this into account, the effect of partial replacement of P<sub>2</sub>O<sub>5</sub> with thermal phosphoric acid containing 1% ammonium nitrate on sulfuric acid was studied. The conditions are the same as in the absence of ammonium nitrate. The results of the decomposition of tricalcium phosphate with thermal acid containing 1% ammonium nitrate and the replacement of 10%, 20% and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid are shown in Table 3.

**Table 3**  
**The effect of partial replacement of phosphoric acid containing ammonium nitrate with sulfuric acid on the chemical composition of the pulp**

№	Performance	Content of components, wt. %								
		when replacing H <sub>3</sub> PO <sub>4</sub> with H <sub>2</sub> SO <sub>4</sub> , %								
		10	20	30	10	20	30	10	20	30
1.	Initial concentration of P <sub>2</sub> O <sub>5</sub> in WPPA, %	18,07	16,29	14,45	27,11	24,44	21,68	36,14	32,57	28,91
2.	Initial concentration of	1,13	2,30	3,50	1,69	3,45	5,25	2,26	4,59	6,99



	SO <sub>3</sub> in WPPA, %									
3.	Content in the product:									
	P <sub>2</sub> O <sub>5</sub> (total), %	23,06	21,66	20,22	31,73	29,79	27,78	39,09	36,64	34,16
	P <sub>2</sub> O <sub>5</sub> (assimilable), %	21,75	20,73	19,81	30,24	28,63	27,06	38,62	36,31	33,90
	P <sub>2</sub> O <sub>5</sub> (water-soluble), %	20,04	19,44	18,53	27,65	26,88	25,54	35,44	33,88	32,49
	SO <sub>3</sub> (total), %	0,93	1,88	2,86	1,27	2,59	3,92	1,57	3,17	4,82
	SO <sub>3</sub> (water-soluble), %	0,39	0,66	0,81	0,54	0,92	1,09	0,68	1,13	1,34
	CaO (total), %	9,74	9,86	9,97	13,40	13,55	13,70	16,52	16,68	16,84
	CaO (total), %	3,11	2,93	2,53	4,26	4,05	3,08	5,36	4,59	3,91
	влага, %	56,48	57,12	57,80	40,48	41,41	42,41	26,92	28,16	29,42
4.	(P <sub>2</sub> O <sub>5</sub> <sub>assimilable</sub> :P <sub>2</sub> O <sub>5</sub> <sub>total</sub> )×100, %	94,32	95,70	97,97	95,30	96,10	97,40	98,80	99,10	99,24
5.	(P <sub>2</sub> O <sub>5</sub> <sub>water-soluble</sub> :P <sub>2</sub> O <sub>5</sub> <sub>total</sub> )×100, %	86,90	89,75	91,64	87,14	90,23	91,94	90,66	92,47	95,11
6.	K <sub>s</sub> of P <sub>2</sub> O <sub>5</sub> assimilable, %	84,10	88,83	95,85	86,84	89,87	94,69	96,64	97,66	98,45
7.	K <sub>ext</sub> for CaO in aqueous solution, %	31,93	29,72	25,38	31,79	29,89	22,48	32,45	27,52	23,22
8.	Degree of extraction of SO <sub>3</sub> into aqueous solution (Degree of conversion of calcium sulfate), %	41,94	35,11	28,32	42,52	35,52	27,81	43,31	35,65	27,80

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The introduction of 1% ammonium nitrate into the original phosphoric acid with a content of 20% P<sub>2</sub>O<sub>5</sub> and the replacement of 10% P<sub>2</sub>O<sub>5</sub> with sulfuric acid leads to a decrease in P<sub>2</sub>O<sub>5</sub> to 18.07%, which contains 1.13% SO<sub>3</sub>.

Chemical analysis of the pulp for the content of the main components showed that when tricalcium phosphate is decomposed by thermal phosphoric acid with an initial concentration of 18.07% P<sub>2</sub>O<sub>5</sub> and containing 1.13% SO<sub>3</sub>, the content of P<sub>2</sub>O<sub>5</sub><sub>total</sub> is 23.06%, P<sub>2</sub>O<sub>5</sub><sub>assimilable</sub> 21.75%, P<sub>2</sub>O<sub>5</sub><sub>water-soluble</sub> 20, 04%.

With an increase in the amount of replacement of P<sub>2</sub>O<sub>5</sub> with sulfuric acid, the content of P<sub>2</sub>O<sub>5</sub><sub>total</sub> decreases to 21.66% and 20.22%, respectively, when 20 and 30% of P<sub>2</sub>O<sub>5</sub> are replaced with sulfuric acid. The

decomposition coefficient of tricalcium phosphate increases from 84.10% to 88.83% and 95.85%.

With an increase in the content of H<sub>2</sub>SO<sub>4</sub> in phosphoric acid, the proportion of the water-soluble form of SO<sub>3</sub> in the pulp decreases.

Table 4 shows the results of the process of drying the decomposition products of tricalcium phosphate with 20% thermal phosphoric acid when replacing 10%, 20% and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid.

The table shows that the decomposition coefficient is 85.72%, 89.87% and 96.10% when replacing 10%, 20% and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid.



**Table 4**

**Effect of partial replacement of phosphoric acid containing ammonium nitrate with sulfuric acid on the chemical composition of the product**

№	Performance	Content of components, wt. %								
		when replacing H <sub>3</sub> PO <sub>4</sub> with H <sub>2</sub> SO <sub>4</sub> , %								
		10	20	30	10	20	30	10	20	30
1.	Initial concentration of P <sub>2</sub> O <sub>5</sub> in WPPA, %	18,07	16,29	14,45	27,11	24,44	21,68	36,14	32,57	28,91 <sup>3350</sup>
2.	Initial concentration of SO <sub>3</sub> in WPPA, %	1,13	2,30	3,50	1,69	3,45	5,25	2,26	4,59	6,99
3.	Content in the product:									
	P <sub>2</sub> O <sub>5</sub> (total), %	52,15	49,21	47,06	52,27	49,35	46,83	52,76	49,91	47,92
	P <sub>2</sub> O <sub>5</sub> (assimilable), %	49,49	47,29	46,16	50,07	47,79	46,01	52,36	49,66	47,80
	P <sub>2</sub> O <sub>5</sub> (water-soluble), %	45,42	44,26	43,41	45,99	45,03	43,19	48,04	46,63	46,07
	SO <sub>3</sub> (total), %	2,10	4,27	6,66	2,09	4,29	6,61	2,12	4,32	6,76
	SO <sub>3</sub> (water-soluble), %	0,94	1,52	1,95	0,91	1,57	1,90	0,94	1,58	1,94
	CaO (total), %	22,03	22,40	23,20	22,07	22,45	23,10	22,30	23,73	23,63
	CaO (total), %	7,20	6,77	6,10	7,23	6,94	5,31	7,42	6,76	5,72
	влага, %	1,57	2,58	1,79	1,95	2,94	2,91	1,37	2,15	0,98
4.	$(\frac{P_{2O_5\text{assimilable}}}{P_{2O_5\text{total}}}) \times 100$ , %	94,90	96,10	98,09	95,79	96,84	98,25	99,24	99,50	99,75
5.	$(\frac{P_{2O_5\text{water-soluble}}}{P_{2O_5\text{total}}}) \times 100$ , %	87,11	89,94	92,24	87,99	91,25	92,23	91,05	93,43	96,14
6.	K <sub>s</sub> of P <sub>2</sub> O <sub>5</sub> assimilable, %	85,72	89,87	96,10	88,21	91,79	96,42	97,87	98,80	99,45
7.	K <sub>ext</sub> for CaO in aqueous solution, %	32,68	30,22	26,29	32,76	30,91	22,99	33,27	28,50	24,21
8.	Degree of extraction of SO <sub>3</sub> into aqueous solution (Degree of conversion of calcium sulfate), %	44,76	35,60	29,28	43,54	36,60	28,74	44,34	36,57	28,70

The use of more concentrated phosphoric acid with the replacement of 10.20 and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid makes it possible to obtain a product with a higher degree of decomposition. With an increase in the proportion of sulfuric acid to 20%, the degree of decomposition increases to 91.79% and to 96.42% when 30% P<sub>2</sub>O<sub>5</sub> is replaced by sulfuric acid. The highest results of the decomposition coefficient were obtained when phosphoric acid was evaporated to a content of 32.57% P<sub>2</sub>O<sub>5</sub> and 4.59% SO<sub>3</sub>, as well as up to 28.91% P<sub>2</sub>O<sub>5</sub> and 6.99% SO<sub>3</sub>, respectively, 98.80% and 99.45%.

**CONCLUSION.**

The use of more concentrated phosphoric acid with the replacement of 10, 20 and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid makes it possible to obtain a product with a higher degree of decomposition. The highest results of the decomposition coefficient were obtained when phosphoric acid was evaporated to a content of 32.90% P<sub>2</sub>O<sub>5</sub> and 4.64% SO<sub>3</sub>, as well as up to 29.20% P<sub>2</sub>O<sub>5</sub> and 7.06% SO<sub>3</sub>, respectively, 97.92% and 99.51%.

Decomposition of tricalcium phosphate with thermal acid containing 1% ammonium nitrate and replacement of 10%, 20% and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid. The highest results of the decomposition coefficient were obtained



when phosphoric acid was evaporated to a content of 32.57% P<sub>2</sub>O<sub>5</sub> and 4.59% SO<sub>3</sub>, as well as up to 28.91% P<sub>2</sub>O<sub>5</sub> and 6.99% SO<sub>3</sub>, respectively, 98.80% and 99.45% .

The use of more concentrated phosphoric acid with the replacement of 10, 20 and 30% P<sub>2</sub>O<sub>5</sub> with sulfuric acid makes it possible to obtain a product with a higher degree of decomposition. The best indicators of the degree of transition of SO<sub>3</sub> into a water-soluble form are observed when using a mixture of acids containing ammonium nitrate.

#### LITERATURE

1. Arislanov A.S. Development of technology for obtaining calcium-containing nitrogen-phosphorus fertilizers with a water-soluble form of sulfates from phosphorites of Karatau and Central Kyzylkum: Diss. ... cand. tech. Sciences. - Namangan-2022. - 127p.

2. Shamshidinov I.T. Development of an improved technology for the production of extractive phosphoric acid and the production of concentrated phosphorus-containing fertilizers from phosphorites of Karatau and Central Kyzyl Kum: Diss. ... doc. tech. Sciences. - Tashkent: IGIC AS RUz, 2017. - 193 p.

3. Gafurov K., Shamshidinov I.T., Arislanov A.S. Sulfuric acid processing of high-magnesian phosphates and obtaining NPS-fertilizers based on them // Monograph. - Namangan: Publishing house "Istedodziyo press", 2020. - 136 p.

4. Gafurov K. Fluorine-free fertilizers from Karatau phosphorites Tashkent: FAN, 1992. - 200 p.

7. Gafurov K., Shamshidinov I. T., Arislanov A. S. Sulfuric acid processing of Karatau phosphorites and complex fertilizers based on them. Monograph. 2020 LAMBERT Academic Publishing. – 132 p.

8. Gafurov K., Arislanov A., Shamshidinov I. Reduction of fluoride compounds in phosphogypsum // Scientific and technical journal FerPI. - Fergana, 2004. - No. 3. - P. 63-66.

9. Gafurov K., Shamshidinov. I.T., Arislanov A.S. Defluorination of extraction phosphoric acid in the process of its extraction. Vestnik FerPI, Fergana, 2005, No. 1

10. Gafurov K., Arislanov A., Shamshidinov I. Reduction of fluoride compounds in phosphogypsum // Scientific and technical journal FerPI. - Fergana, 2004. - No. 3. - P. 63-66.

11. Gafurov K. Resource saving and improvement of ecological cleanliness of Karatau phosphorite processing products. Abstract dis. ... doc. tech. Sciences. – Tashkent, 1990.–52 p.

12. Arislanov A.S., Rezhabbaev M., Soliev M., Abdurazzakova M. Defluorination of EPA during its extraction. Scientific electronic journal "Academic journalism". – Ufa: Aeterna, Russia-2018.-p.25

13. Arislanov A.S., Zhuraboev F., Juraev M. Defluorination of EPA of Kyzylkum phosphorites during decomposition: Collection of articles on the results of the International Scientific and Practical Conference (Chelyabinsk, May 26, 2018). in Part 1 - Sterlitamak: AMI, 2018. - 267 p.

14. Patent No. 5698 UZ. Method for obtaining extraction phosphoric acid /Gafurov K., Shamshidinov I.T., Arislanov A., Mamadaliev A. (UZ)/1998. - Bull. N4.

15. Gafurov K. Resource saving and improvement of ecological cleanliness of Karatau phosphorite processing products. Dis. ... doc. tech. Sciences. - Tashkent, 1990. - 52 p.

16. Arislanov A.S., Shamshidinov I.T., Gafurov K. Calcium-containing nitrogen-phosphorus fertilizers with soluble sulfates // Uzbek Chemical Journal. - Tashkent, 2005. - No. 4. - S. 9-13. (02.00.00. №6)

17. Arislanov A.S., Shamshidinov I.T. Combined technology for the production of sulfur-containing nitrogen-phosphorus fertilizer// Composite materials. Uzbek scientific, technical and industrial journal. - Tashkent, 2018. - No. 3. - P. 56-57. (02.00.00. №4)



18. Arislanov Akmaljon Sayubbaevich, Shamshidinov Israiljon Turgunovich, Ergashev Oybek Karimovich. Phosphoric Acid Decomposition of Phosphorite with Partial Replacement of Its Sulfuric Acid // International Journal of Advanced Research in Science, Engineering and Technology. – 2019. – Vol. 6, – Issue 8. – pp. [10473](#)-10475. (05.00.00. №8)

19. Arislanov, A. S., Rezhabbaev, M., Soliev, M., & Abdurazzakova, M. (2018). Defluorination of EPA during its extraction. Scientific electronic journal "Academic journalism". Ufa: Aeterna, Russia, 25.

20. Arislanov A.S., Zhuraboev F.M., Soliev M.I., Botirov T.T. Method for producing nitrosuperammophos. Scientific electronic journal "Academic journalism". – Ufa: Aeterna, Russia-2018.-p.19-22

21. Arislanov A., Soliev M., Abidov I., Davlatova M. Method for obtaining extraction phosphoric acid from Kizyl-Kum phosphorites. Scientific electronic journal "Academic journalism". – Ufa: Aeterna, Russia-2018.-p.22-24

